



HAL
open science

On Interconnected Observer Design for Nonlinear System

Mei Zhang, Ze-Tao Li, Michel Cabassud, Boutaib Dahhou

► **To cite this version:**

Mei Zhang, Ze-Tao Li, Michel Cabassud, Boutaib Dahhou. On Interconnected Observer Design for Nonlinear System. 2019 International Conference on Modelling, Identification and Control (ICMIC 2019), Jul 2019, Tianjin, China. pp.1313-1323, 10.1007/978-981-15-0474-7_123 . hal-02943938

HAL Id: hal-02943938

<https://laas.hal.science/hal-02943938>

Submitted on 3 Mar 2021

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destinée au dépôt et à la diffusion de documents scientifiques de niveau recherche, publiés ou non, émanant des établissements d'enseignement et de recherche français ou étrangers, des laboratoires publics ou privés.



Open Archive Toulouse Archive Ouverte

OATAO is an open access repository that collects the work of Toulouse researchers and makes it freely available over the web where possible

This is an author's version published in: <https://oatao.univ-toulouse.fr/25954>

Official URL :

https://doi.org/10.1007/978-981-15-0474-7_123

To cite this version:

Zhang, Mei and Li, Ze-tao and Cabassud, Michel and Dahhou, Boutaïeb *On Interconnected Observer Design for Nonlinear System*. (2019) In: 2019 International Conference on Modelling, Identification and Control (ICMIC 2019), 13 July 2019 - 15 July 2019 (Tianjin, China).

Any correspondence concerning this service should be sent to the repository administrator: tech-oatao@listes-diff.inp-toulouse.fr

On Interconnected Observer Design for Nonlinear System

Mei Zhang, Ze-tao Li, Michel Cabassud and Boutaïeb Dahhou

Abstract This paper investigates the possibility of decomposing a control system into an interconnection of actuator and process subsystems; this allows monitoring the properties of the interconnected system globally and locally. For that, observer for the nonlinear interconnected system is studied. Specially, the interconnection between the two subsystems is assumed to be inaccessible to measurement. The aim is then to accurately estimate online the states vector of each subsystem, as well as the unknown interconnection. Numerical simulations confirm the effectiveness of the designed observer.

Keywords Interconnected system · Unknown interconnection · States estimation · Left invertibility · Actuator subsystem · Process subsystem

1 Introduction

In practice, interconnected dynamical systems appear in many control applications whether naturally or intentionally due to control design purpose. An interconnected system consists of a series of interconnected dynamical units, and therefore exhibits very complicate dynamics [1].

M. Zhang · Z. Li (✉)
Electrical Engineering School, Guizhou University, Guiyang 550025, China
e-mail: gzulzt@163.com

M. Zhang
e-mail: mei.zhang@ensiacet.fr

M. Cabassud
CNRS, LGC, 31030 Toulouse, France
e-mail: michel.cabassud@ensiacet.fr

Université de Toulouse, UPS, LGC, 31030 Toulouse, France

B. Dahhou
CNRS, LAAS, 31400 Toulouse, France
e-mail: boutaib.dahhou@laas.fr

Université de Toulouse, UPS, LAAS, 31400 Toulouse, France

https://doi.org/10.1007/978-981-15-0474-7_123

Over the past years, the topic of states estimation for interconnected system has received extensively attention in the literature, see e.g. in [1–3]. A large number of publications focused on this problem with satisfactory results are in a centralized manner, resulting in various types of observers like high gain observer [3], sliding mode observer [4], adaptive observer [5] etc. However, note that a centralized observer may not be practical for the interconnected systems due to the complexity of implementation, and the state or parts of the state cannot be measured due to uneconomic measurement costs or physical circumstances like high temperatures, where no measurement equipment is available, for example. A solution to overcome this difficulty is to decompose the systems into an interconnection of several subsystems so that the observers can be designed in a decentralized manner. A typical approach of state estimation is to design observers for each subsystem individually and the overall estimator is formed by gathering of all the observers, different kinds of methodologies are developed, like in [6–9].

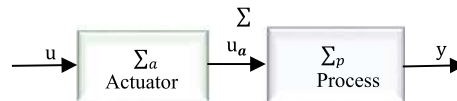
With respect to the above mentioned methods, one major challenge is the availability of the measurement of the interconnections between subsystems. For example, the output of the actuator can be either uneconomic or unrealistic to measure its output. A promising approach was reported in [10] where the problem of state-observation is addressed for nonlinear systems that modeled by an ODE–PDE series association. This problem has also been studied for interconnected system formed by a nonlinear system followed by a linear system, like in [8].

This paper considers the issues of both state and unknown interconnection estimation for the interconnected system represented by two nonlinear associations connected in series. Two underlying issues are worth to be highlighted to better understand the nature of the considered estimation problem. Firstly, the measurement output used in the observer of former subsystem is assumed not accessible; the solution is to replace it by an estimate via observer of latter subsystem. Secondly, in the latter subsystem, the estimated interconnection that provided for the previous subsystem is treated as an additional state, forming a new extended subsystem; and expression for the new state is obtained by computing derivatives of output equation of the previous subsystem.

2 Motivations and Problem Formulations

The problem of states observation is addressed for nonlinear systems that can be modeled by two interconnected nonlinear dynamical units, the actuator and the process subsystems, as shown in Fig. 1. The aim is to accurately estimate the states

Fig. 1 Interconnected system structure



vector of both subsystems, as well as the interconnection.

We consider a dynamical process subsystem as an input affine form:

$$\sum_p : \begin{cases} \dot{x} = f(x) + g(x)u_a, & x(t_0) = x_0 \\ y = h(x) \end{cases} \quad (1)$$

where $x \in \mathfrak{R}^n$ is the state of the process subsystem, $y \in \mathfrak{R}^p$ is the output of the global system, which is also the output of the process subsystem. $u_a \in \mathfrak{R}^m$ is the input of process subsystem, which is also the output of the actuator subsystem. u_a is assumed to be inaccessible. f and g are smooth vector field on \mathfrak{R}^n and h is smooth vector field on \mathfrak{R}^p .

An input affine structure is also assumed for the actuator subsystem:

$$\sum_a : \begin{cases} \dot{x}_a = f_a(x_a) + g_a(x_a)u, & x_a(t_0) = x_{a0} \\ u_a = h_a(x_a) \end{cases} \quad (2)$$

where $x_a \in \mathfrak{R}^n$ is the state, $u \in \mathfrak{R}^1$ is the input, $u_a \in \mathfrak{R}^m$ is the output of the actuator subsystem, which is also the input of the process subsystem. f_a and g_a are smooth vector field on \mathfrak{R}^n and h is smooth vector field on \mathfrak{R}^m .

Considering interconnected system depicted by (1) and (2), it is desirable to monitor the performance of the interconnected system with aspect to individual subsystems and the overall system. However, the major difficulty for employing the existing methods is to satisfy the assumption that inputs and outputs of each subsystem are available, since the connection point between the two blocks is not accessible to measurement. This is because the connection is the output of the actuator subsystem where online measurement is either difficult to obtain due to physical reasons or the measurement is uneconomical since actuators are often far from the controller. As shown in Fig. 1, the particular aim in our design is to accurately estimate online the state vector x and x_a of each subsystem, as well as the unmeasured interconnection vector u_a .

3 Interconnected Observer Design

The structure of the proposed observer is depicted as a two level interconnected observer system which consists of two state estimators, the actuator and the process state estimators. The specific idea of the proposed interconnected observer is as follows. First, an existing observer is supposed to be already available for the nonlinear subsystem \sum_a with measured output u_a , then we implement that observer using an estimate of u_a , denoted by \tilde{u}_a . In order to produce such an estimate, we extend the state space of the process subsystem \sum_p to include u_a as an additional state. By computing derivatives of u_a in actuator subsystem, we can obtain an expression corresponding to times derivatives of the output u_a which is a function of u , derivatives

of u and x_a . Then an observer is constructed for this extended process subsystem. State estimator of actuator subsystem, together with state estimator of process subsystem, a kind of interconnected observer designed method is then proposed for the studied interconnected nonlinear system.

3.1 Observer Design for the Interconnected System

First, consider a converging observer for actuator subsystem is:

$$\begin{cases} \dot{\hat{x}}_a = f_a(\hat{x}_a) + g_a(\hat{x}_a)u + k_a(\varphi_a, \hat{x}_a)(h_a(\hat{x}_a) - u_a) \\ \dot{\hat{\varphi}}_a = G_a(\hat{x}_a, u, \varphi_a) \end{cases} \quad (3)$$

where k_a , G_a are smooth gain functions with respect to their arguments. G_a is a subset of \mathfrak{N}^n . To this end, introduce the state estimation error as:

$$e_a := x_a - \hat{x}_a$$

Then subtracting corresponding equation of (2) and (3), we get the following error dynamics as:

$$\dot{e}_a(t, e_a) = f_a(x_a) + g_a(x_a)u - f_a(\hat{x}_a) - g_a(\hat{x}_a)u - K(u, \hat{x}_a, u_a) \quad (4)$$

where $K(u, \hat{x}_a, u_a) = k_a(\varphi_a, \hat{x}_a)(h_a(\hat{x}_a) - u_a)$.

The observer defined by (3) could be implemented on condition that u_a is accessible, but it is not the fact in the case. Since u_a in our design represents the output of the actuator subsystem which is assumed unmeasured, therefore we have to replace u_a with an estimated \tilde{u}_a by the available measurements.

$$\begin{cases} \dot{\hat{x}}_a = f_a(\hat{x}_a) + g_a(\hat{x}_a)u + k_a(\varphi_a, \hat{x}_a)(h_a(\hat{x}_a) - \tilde{u}_a) \\ \dot{\hat{\varphi}}_a = G_a(\hat{x}_a, u, \varphi_a) \end{cases} \quad (5)$$

denote $K(u, \hat{x}_a, \tilde{u}_a) = k_a(\varphi_a, \hat{x}_a)(h_a(\hat{x}_a) - \tilde{u}_a)$.

We seek again estimation error by subtracting corresponding equation in (2) and (5), thus yielding the new error dynamics as follows:

$$\dot{\tilde{e}}_a(t, \tilde{e}_a) = \dot{e}_a(t, e_a) + K(u, \hat{x}_a, u_a) - K(u, \hat{x}_a, \tilde{u}_a) \quad (6)$$

In order to ensure exponential stability of the error dynamics (6), we need an assumption regarding the sensitivity of $K(u, \hat{x}_a, u_a)$ with respect to changes in u_a . The following Assumption provides a sufficient condition for achieving this purpose. This subject of following statement is inspired by [8].

Assumption 1 for any $u \in \mathbb{U}$, $(t, \hat{x}_a, \hat{u}_a) \in \mathcal{A.C}(\mathbb{R}^+, \mathbb{R})$, there exists a real constant γ_3 satisfies:

$$\|K(u, \hat{x}_a, u_a) - K(u, \hat{x}_a, \tilde{u}_a)\| \leq \gamma_3 \|u_a - \tilde{u}_a\| \quad (7)$$

Assumption 2 implies that the definition of $\tilde{e}_a(t, \tilde{e}_a)$ in (6) is not affected.

Theorem 1 if Assumption 1 is satisfied, then the observer described in (5) is an exponential observer for the actuator subsystem described in (2).

3.2 State Estimator Design for Process Subsystem

In order to produce an observer for the process subsystem (1) subject to unknown inputs, we solve this problem by extending this unknown input as an additional state, and propose an observer for the extended system.

Let:

$$x_u \triangleq u_a \quad \dot{x}_u = \dot{u}_a$$

According to [8], we define a function $\varepsilon(u, \dot{u}, x_a)$ with respect to the time derivative of the output u_a in (2).

$$\dot{x}_u = \varepsilon(u, \dot{u}, x_a) = \frac{\partial h_a}{\partial u}(u, x_a)\dot{u} + \frac{\partial h_a}{\partial x_a}(u, x_a)f_a(u, x_a) \quad (8)$$

Assumption 2 For any $u \in \mathbb{U}$, $(t, \hat{x}_a) \in \mathcal{A.C}(\mathbb{R}^+, \mathbb{R})$, there exists a real constant γ_4 satisfies:

$$\|\varepsilon(u, \dot{u}, \hat{x}_a) - \varepsilon(u, \dot{u}, x_a)\| \leq \gamma_4 \|x_a - \hat{x}_a\|$$

Similar to Assumptions 1 and 2 implies global Lipchitz-type condition on function ε , and it can also be replaced by local smoothness condition since u, \dot{u}, x_a are bounded in physical problem.

Then new actuator and new process subsystem can be expressed as:

$$\sum_p : \begin{cases} \dot{x} = f(x) + g(x)x_u \\ \dot{x}_u = \varepsilon(u, \dot{u}, x_a) \end{cases} \quad (9)$$

Define $z = [z_1 \ z_2] = [x \ x_u]$, then system (9) can be extended as:

$$\begin{cases} \dot{z} = l(z_1)G(z_1)z + F(z_1) + \bar{\varepsilon}(u, \dot{u}, x_a) \\ y = Cx \end{cases} \quad (10)$$

where: $G(z_1) = \begin{pmatrix} 0 & g_1(z_1) \\ 0 & 0 \end{pmatrix}$, $F(x_1) = \begin{pmatrix} f_1(z_1) \\ 0 \end{pmatrix}$, $C = (I_n \ 0)$, $\bar{\varepsilon}(u, \dot{u}, x_a) = [0 \ \varepsilon(u, \dot{u}, x_a)]^T$, I_n is $n \times n$ identity matrix, $l(z_1)$ is a scalar real function with respect to their arguments and $\alpha_1 \leq |l(z_1)| \leq \beta_1$.

An extended high gain observer for (10) can be given in the following way:

$$\begin{cases} \dot{\hat{z}} = l(\hat{z}_1)G(\hat{z}_1)\hat{z} + F(\hat{z}_1) + \bar{\varepsilon}(u, \dot{u}, \hat{x}_a) + H(\hat{z}_1)(\hat{y} - y) \\ \hat{y} = C\hat{z} \end{cases} \quad (11)$$

where: $H = [H_{z_1} \ H_{z_2}]^T = \Lambda^{-1}(\hat{z}_1)S_0^{-1}C^T$, $\Lambda(\hat{z}_1) = \begin{bmatrix} I & 0 \\ 0 & G_1(\hat{z}_1) \end{bmatrix}$

3.3 Interconnected Observer

System (5), together with (11), constitutes the interconnected observer for the studied interconnected system, as follows:

$$\begin{cases} \dot{\hat{x}}_a = f_a(\hat{x}_a, u) + k_a(g_a, \hat{x}_a)(h_a(\hat{x}_a) - \hat{z}_2) \\ \dot{\hat{z}} = l(\hat{z}_1)G(\hat{z}_1)\hat{z} + F(\hat{z}_1) + \bar{\varepsilon}(u, \dot{u}, \hat{x}_a) + H(\hat{z}_1)(\hat{y} - y) \end{cases} \quad (12)$$

where virtual measurement \tilde{u}_a in (6) is replaced by its estimation \hat{z}_2 .

4 Numerical Simulations Result

In order to test the performance of the proposed observers, A case study is developed on an intensified HEX reactor. More relative information could be found in [11].

4.1 System Modelling

The actuator subsystem model is described as: $x_a^T = [x_{a1} \ x_{a2} \ x_{a3} \ x_{a4}] = [X_1 \ \frac{dX_1}{dt} \ X_2 \ \frac{dX_2}{dt}]$, $u^T = [u_1 \ u_2] = [p_{c1} \ p_{c2}]$, $u_a^T = [F_1 \ F_2] = [C_v \sqrt{\frac{\Delta P_1}{sg}} X_1 \ C_v \sqrt{\frac{\Delta P_2}{sg}} X_2]$, $C = [c_1 \ c_2 \ c_3 \ c_4] = [C_v \sqrt{\frac{\Delta P_1}{sg}} \ 0 \ C_v \sqrt{\frac{\Delta P_2}{sg}} \ 0]$

where F is flow rate (m^3s^{-1}), ΔP is the fluid pressure drop across the valve (Pa), sg is specific gravity of fluid, X is the valve opening, C_v is valve coefficient A_a is the diaphragm area, p_c is the pneumatic pressure, m is the mass of the control valve stem, μ is the friction of the valve stem, k is the spring compliance, the actuator

subsystem is then described as:

$$\begin{cases} \dot{x}_a = \begin{bmatrix} 0 & 1 & 0 & 0 \\ -\frac{k_1}{m} & -\frac{\mu_1}{m} & 0 & 0 \\ 0 & 0 & 0 & 1 \\ 0 & 0 & -\frac{k_2}{m} & -\frac{\mu_2}{m} \end{bmatrix} x_a + \begin{bmatrix} \frac{A_a}{m} & 0 \\ 0 & 0 \\ 0 & \frac{A_a}{m} \\ 0 & 0 \end{bmatrix} u \\ u_a = \begin{bmatrix} C_v \sqrt{\frac{\Delta P_1}{sg}} & 0 & C_v \sqrt{\frac{\Delta P_2}{sg}} & 0 \end{bmatrix} x_a \end{cases} \quad (13)$$

For the process subsystem, define the state vector as $x^T = [x_1, x_2]^T = [T_p, T_u]^T$, the control input $u_a^T = [u_{a1}, u_{a2}]^T = [F_p, F_u]^T$, the output vector of measurable variables $y^T = [y_1, y_2]^T = [T_p, T_u]^T$, where ρ_p, ρ_u are density of the process fluid and utility fluid (in kg m^{-3}), V_p, V_u are volume of the process fluid and utility fluid (in m^3), c_{pp}, c_{pu} are specific heat of the process fluid and utility fluid (in $\text{J kg}^{-1} \text{K}^{-1}$), U is the overall heat transfer coefficient (in $\text{J m}^{-2} \text{K}^{-1} \text{s}^{-1}$). A is the reaction area (in m^2). F_p, F_u are mass flowrate of process fluid and utility fluid (in kg s^{-1}). T_p is the process fluid temperature. T_u is the utility fluid temperature of previous cell. T_{pi}, T_{ui} are the inlet temperature of process fluid and utility fluid.

Then the process subsystem can be described in the following state-space form:

$$\begin{cases} \dot{x} = f(x) + \sum_{i=1}^2 g_i(x) u_a \\ y = h(x, u_a) \end{cases} \quad (14)$$

where $f(x) = \begin{pmatrix} f_1(x) \\ f_2(x) \end{pmatrix} = \begin{pmatrix} \frac{h_p A}{\rho_p c_{pp} V_p} (T_p - T_u) \\ \frac{h_u A}{\rho_u c_{pu} V_u} (T_u - T_p) \end{pmatrix}$, and $g(x) = (g_1, g_2) = \begin{pmatrix} \frac{(T_{pi} - T_p)}{V_p} & 0 \\ 0 & \frac{(T_{ui} - T_u)}{V_u} \end{pmatrix}$, $y_1 = x_1, y_2 = x_2$.

By using (8), we can obtain a function for the derivatives for u_a :

$$\begin{aligned} \dot{u}_a &= \varepsilon(u, \dot{u}, x_a) = \frac{\partial h_a}{\partial u}(u, x_a) \dot{u} + \frac{\partial h_a}{\partial x_a}(u, x_a) f_a(u, x_a) \\ &= \left(C_v \sqrt{\frac{\Delta P_1}{sg}} \ 0 \ C_v \sqrt{\frac{\Delta P_2}{sg}} \ 0 \right) x_a + \left(\frac{A_a}{m} C_v \sqrt{\frac{\Delta P_1}{sg}} \ \frac{A_a}{m} C_v \sqrt{\frac{\Delta P_2}{sg}} \right) u \end{aligned} \quad (15)$$

Define the state vector as $x_1^T = [x_{11}, x_{12}]^T = [T_p, T_u]^T$, unmeasured state $x_2^T = [x_{21}, x_{22}]^T = [u_{a1}, u_{a2}]^T = [F_p, F_u]^T$, the output vector of measurable variables $y^T = [y_1, y_2]^T = [T_p, T_u]^T$, then the Eqs. (14) and (15) can be rewritten in the following state-space form:

$$\begin{cases} \dot{x}_1 = G_1(x_1)x_2 + g_1(x_1, u) \\ \dot{x}_2 = \varepsilon(u, \dot{u}, x_a) \\ y = x_1 \end{cases} \quad (16)$$

where, $G_1(x_1) = \begin{pmatrix} \frac{(T_{pi}-x_{11})}{V_p} & 0 \\ 0 & \frac{(T_{ui}-x_{12})}{V_u} \end{pmatrix}$, and $f_1(x) = \begin{pmatrix} \frac{h_p A}{\rho_p C_{pp} V_p} (x_{11} - x_{12}) \\ \frac{h_u A}{\rho_u C_{pu} V_u} (x_{12} - x_{11}) \end{pmatrix}$.

4.2 Simulation Results

Numerical simulations were carried out. Considering the actuator and process model given by (13) and (16), observers (12) were designed for estimating unmeasured inlet flows F_p , F_u , and monitoring performance final product T_p , T_u . An initial value $F_u = 4.22e^{-5}m^3s^{-1}$, and $F_p = 4.17e^{-6}m^3s^{-1}$ were considered, then followed by an abrupt change of F_u at $t = 60$ s. After that, at $t = 100$ s, F_p begins to deteriorate. Simulation Results are illustrated in Figs. 2, 3, 4 and 5.

From Figs. 2 and 3, after a short transient time, the estimated outlet fluid temperature \hat{T}_p and \hat{T}_u in dash line give an accurate estimation value to the measurement T_p and T_u in solid line. At 60 s, the estimated \hat{T}_p unexpectedly decrease, and finally it stabilizes at a new level, a drop of 0.2 °C is occurred, then another drops happens at $t = 100$ s before it reaches the new stable level with another 0.9 °C reduction. The

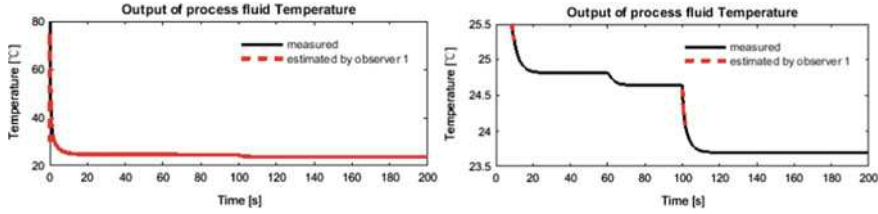


Fig. 2 Outlet temperature of process fluid, solid line denotes measured value T_p while dash line is the estimated one \hat{T}_p

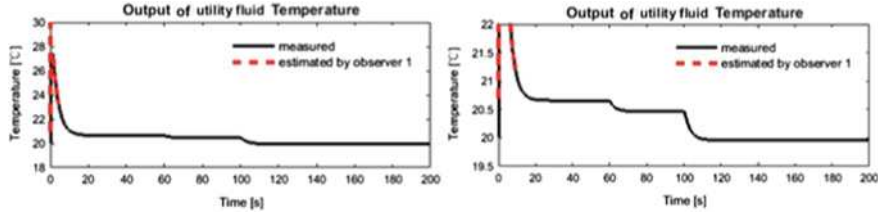


Fig. 3 Outlet temperature of utility fluid, solid line denotes measured value T_u while dash line is the estimated one \hat{T}_u

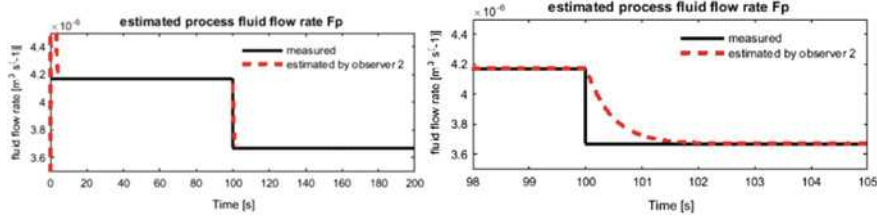


Fig. 4 The computation and estimation of process fluid flow rate; solid line is the computed value F_p , dash line is the estimated one \hat{F}_p

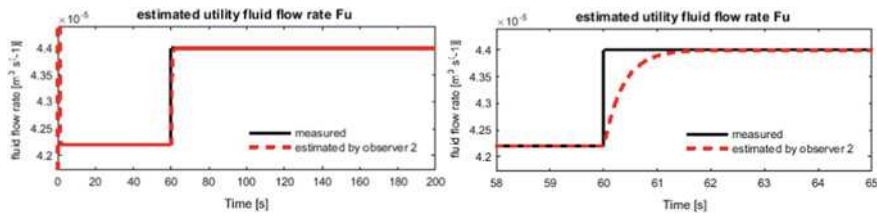


Fig. 5 The computation and estimation of utility fluid flow rate; solid line is the computed value F_u , dash line is the estimated one \hat{F}_u

similar result is obtained in the estimated \hat{T}_u of utility fluid in Fig. 3. It is shown that the measured T_u drops 0.2 and 0.5 °C at 60 s, 100 s respectively. The estimated \hat{T}_u in dash line tracks T_u after observer converges. The simulation curve indicates that the observer proposed is proper for tracking system performances.

As shown in Fig. 4, in the first place, the estimated process fluid flow rate \hat{F}_p in dash line converges to the simulated value F_p in solid line after transient response. After that, at 100 s, the simulated F_p in solid line decrease unexpectedly, fortunately, the estimated value in dash curve gives a quick response to the variation, and it takes 1.5 s to track F_p again. The decrease implies parameter changes in process fluid actuator which satisfied the assumption. Figure 5 demonstrates the results for utility fluid flow rate. At time 60 s, as expected, the simulated utility fluid flow rate in solid line jumps. It also proves in Fig. 5 that the estimated utility fluid flow rate \hat{F}_p in dash line tracks well F_p in solid line.

Now, it is clear that the proposed interconnected observer is effective even the unknown connection is time-varying either individually or simultaneously. Therefore the proposed observer proves the capacity of performance monitoring, as well as estimation of unknown connection of an interconnected system.

5 Conclusion

The paper considers the issues of both state and unmeasured interconnection estimation for a class of interconnected dynamic system. To achieve this purpose, the unknown outputs information of the latter subsystem are replaced by their estimation through the observer proposed in the former subsystem. Moreover, an extended high gain observer is considered to exactly estimate the states of the former subsystem subject to unknown inputs. While through computing the derivatives of the output vectors in the latter subsystem, the unknown input can be expressed as a function of the inputs, derivatives of the inputs and the states of the actuator subsystem. Numerical simulation examples are given to illustrate the effectiveness of the proposed methods.

Acknowledgements This work was supported by Science and Technology Foundation of Guizhou Province, China ([2016]1053), and Key Project of Science and Technology Foundation of Guizhou Province, China ([2016]2302). And [2017]5788.

References

1. Yang, J., Zhu, F., Yu, K., Bu, X.: Observer-based state estimation and unknown input reconstruction for nonlinear complex dynamical systems. *Commun. Nonlinear Sci. Numer. Simul.* **20**(3), 927–939 (2015)
2. Besançon, G., Hammouri, H.: On observer design for interconnected systems. *J. Math. Syst. Estimation Control* **8**(3), 1–26 (1998)
3. Vijay, P., Tade, M.O., Ahmed, K., Utikar, R., Pareek, V.: Simultaneous estimation of states and inputs in a planar solid oxide fuel cell using nonlinear adaptive observer design. *J. Power Sources* **248**, 1218–1233 (2014)
4. Djeghali, N., Djennoune, S., Bettayeb, M., Ghanes, M., Barbot, J.P.: Observation and sliding mode observer for nonlinear fractional-order system with unknown input. *ISA Trans.* **63**, 1–10 (2015)
5. Farza, M., M'Saad, M., Menard, T., Fall, M.L., Gehan, O., Pigeon, E.: Simple cascade observer for a class of nonlinear systems with long output delays. *IEEE Trans. Automat. Control* **60**, 3338–3343 (2015)
6. Keliris, C., Polycarpou, M.M., Parisini, T.: A robust nonlinear observer-based approach for distributed fault detection of input-output interconnected systems. *Automatica* **53**, 408–415 (2015)
7. Sandberg, H., André, H., Johansson, K.H.: Distributed fault detection for interconnected second-order systems with applications to power networks consensus protocols in practice. In: *First Workshop on Secure Control Systems (SCS)*, Stockholm (2010)
8. Grip, H.F., Saberi, A., Johansen, T.A.: Observers for interconnected nonlinear and linear systems. *Automatica* **48**(7), 1339–1346 (2012)

9. Dashkovskiy, S., Naujok, L.: Quasi-ISS/ISDS observers for interconnected systems and applications. *Syst. Control Lett.* **77**, 11–21 (2015)
10. Antonio Susto, G., Krstic, M.: Control of PDE-ODE cascades with Neumann interconnections. *J. Franklin Inst.* **347**(1), 284–314 (2010)
11. Théron, F., Anxionnaz-Minvielle, Z., Cabassud, M., Gourdon, C., Tochon, P.: Characterization of the performances of an innovative heat-exchanger/reactor. *Chem. Eng. Process. Process Intensification* **82**, 30–41 (2014)